

"ME 345 Local and Average Convection Coefficient"**"Example Problem 6.4 from 6th Edition Incropera and DeWitt"****"Given Information"**

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L$ = 'water'
T_1 = 300 [K]
T_2 = 350 [K]
P = 101 [kPa]
u_infinity = 1 [m/sec]
h_lam_300 = C_lam_300*x^(-0.5)
h_turb_300 = C_turb_300*x^(-0.2)
h_lam_350 = C_lam_350*x^(-0.5)
h_turb_350 = C_turb_350*x^(-0.2)

C_lam_300 = 395 [W/(K*(m^1.5))]
C_turb_300 = 2330 [W/(K*(m^1.8))]
C_lam_350 = 477 [W/(K*(m^1.5))]
C_turb_350 = 3600 [W/(K*(m^1.8))]

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\$IFNOT Parametric Table

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x=0.6 [m]
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$endif
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"Properties"

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rho_300 = 1/volume(L$, T=T_1, P=P)
mu_300 = viscosity(L$, T=T_1, P=P)
rho_350 = 1/volume(L$, T=T_2, P=P)
mu_350 = viscosity(L$, T=T_2, P=P)

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"Calculating Transition Location"

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Re_x_c_low = 10^5 [dim]
Re_x_c_mid = 5*10^5 [dim]
Re_x_c_high = 3*10^6 [dim]

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x_c_300_low = (Re_x_c_low*mu_300)/(rho_300*u_infinity)
x_c_300_mid = (Re_x_c_mid*mu_300)/(rho_300*u_infinity)
x_c_300_high = (Re_x_c_high*mu_300)/(rho_300*u_infinity)

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x_c_350_low = (Re_x_c_low*mu_350)/(rho_350*u_infinity)
x_c_350_mid = (Re_x_c_mid*mu_350)/(rho_350*u_infinity)
x_c_350_high = (Re_x_c_high*mu_350)/(rho_350*u_infinity)

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"Calculating Average Convection Coefficients"

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h_bar_300_low = 1/x*((C_lam_300/0.5*(x_c_300_low^0.5)) + C_turb_300/0.8*(x^0.8 - x_c_300_low^0.8))
h_bar_300_mid = 1/x*((C_lam_300/0.5*(x_c_300_mid^0.5)) + C_turb_300/0.8*(x^0.8 - x_c_300_mid^0.8))
h_bar_300_high = 1/x*((C_lam_300/0.5*(x^0.5)))

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h_bar_350_low = 1/x*((C_lam_350/0.5*(x_c_350_low^0.5)) + C_turb_350/0.8*(x^0.8 - x_c_350_low^0.8))
h_bar_350_mid = 1/x*((C_lam_350/0.5*(x_c_350_mid^0.5)) + C_turb_350/0.8*(x^0.8 - x_c_350_mid^0.8))
h_bar_350_high = 1/x*((C_lam_350/0.5*(x^0.5)))

```

SOLUTION**Unit Settings: SI K kPa kJ mass deg**

C _{lam,300} = 395 [W/(K*(m ^{1.5}))]	C _{lam,350} = 477 [W/(K*(m ^{1.5}))]
C _{turb,300} = 2330 [W/(K*(m ^{1.8}))]	C _{turb,350} = 3600 [W/(K*(m ^{1.8}))]
$\bar{h}_{300,high}$ = 1020 [W/(K*m ²)]	$\bar{h}_{300,low}$ = 2931 [W/(K*m ²)]
$\bar{h}_{300,mid}$ = 1624 [W/(K*m ²)]	$\bar{h}_{350,high}$ = 1232 [W/(K*m ²)]
$\bar{h}_{350,low}$ = 4747 [W/(K*m ²)]	$\bar{h}_{350,mid}$ = 3695 [W/(K*m ²)]

$h_{lam,300} = 509.9$ [W/(K*m²)]
 $h_{turb,300} = 2581$ [W/(K*m²)]
 L\$ = 'water'
 $\mu_{350} = 0.0003688$ [N-sec/m²]
 $Re_{x,c,high} = 3.000E+06$
 $Re_{x,c,mid} = 500000$
 $\rho_{350} = 973.7$ [kg/m³]
 $T_2 = 350$ [K]
 $x = 0.6$ [m]
 $x_{c,300,low} = 0.08568$ [m]
 $x_{c,350,high} = 1.136$ [m]
 $x_{c,350,mid} = 0.1894$ [m]

$h_{lam,350} = 615.8$ [W/(K*m²)]
 $h_{turb,350} = 3987$ [W/(K*m²)]
 $\mu_{300} = 0.0008538$ [N-sec/m²]
 $P = 101$ [kPa]
 $Re_{x,c,low} = 100000$
 $\rho_{300} = 996.6$ [kg/m³]
 $T_1 = 300$ [K]
 $u_{\infty} = 1$ [m/sec]
 $x_{c,300,high} = 2.57$ [m]
 $x_{c,300,mid} = 0.4284$ [m]
 $x_{c,350,low} = 0.03787$ [m]

No unit problems were detected.

KEY VARIABLES

$x_{c,300,low} = 0.08568$ [m]
 $x_{c,300,mid} = 0.4284$ [m]
 $x_{c,300,high} = 2.57$ [m]
 $\bar{h}_{300,low} = 2931$ [W/(K*m²)]
 $\bar{h}_{300,high} = 1020$ [W/(K*m²)]
 $\bar{h}_{300,mid} = 1624$ [W/(K*m²)]
 $x_{c,350,low} = 0.03787$ [m]
 $x_{c,350,mid} = 0.1894$ [m]
 $x_{c,350,high} = 1.136$ [m]
 $\bar{h}_{350,low} = 4747$ [W/(K*m²)]
 $\bar{h}_{350,mid} = 3695$ [W/(K*m²)]
 $\bar{h}_{350,high} = 1232$ [W/(K*m²)]

Parametric Table: Table 2

	x	$h_{lam,350}$	$h_{turb,350}$
	[m]	[W/(K*m ²)]	[W/(K*m ²)]
Run 1	0.001	15084	14332
Run 2	0.025	3017	7529
Run 3	0.05	2133	6554
Run 4	0.075	1742	6044
Run 5	0.1	1508	5706
Run 6	0.125	1349	5457
Run 7	0.15	1232	5261
Run 8	0.175	1140	5101
Run 9	0.2	1067	4967
Run 10	0.225	1006	4851
Run 11	0.25	954	4750
Run 12	0.275	909.6	4661
Run 13	0.3	870.9	4580
Run 14	0.325	836.7	4507
Run 15	0.35	806.3	4441
Run 16	0.375	778.9	4380
Run 17	0.4	754.2	4324
Run 18	0.425	731.7	4272
Run 19	0.45	711.1	4223
Run 20	0.475	692.1	4178
Run 21	0.5	674.6	4135

Parametric Table: Table 2

	x [m]	$h_{lam,350}$ [W/(K*m ²)]	$h_{turb,350}$ [W/(K*m ²)]
Run 22	0.525	658.3	4095
Run 23	0.55	643.2	4057
Run 24	0.575	629	4021
Run 25	0.6	615.8	3987

