

**GIVEN:** Water at  $T = 300^\circ\text{F}$ ,  $p = 500$  psia  
**FIND:**  $v, \rho, u, h, s$

**GIVEN:** R-22 at  $T = 200^\circ\text{F}$ ,  $p = 120$  psia  
**FIND:**  $v, u, h$

**GIVEN:** Ammonia at  $T = -30^\circ\text{F}$   
**FIND:** The vapor pressure,  $p_{sat}$  and  $h_{fg}$

**GIVEN:** R-134a  
**FIND:** The normal boiling point

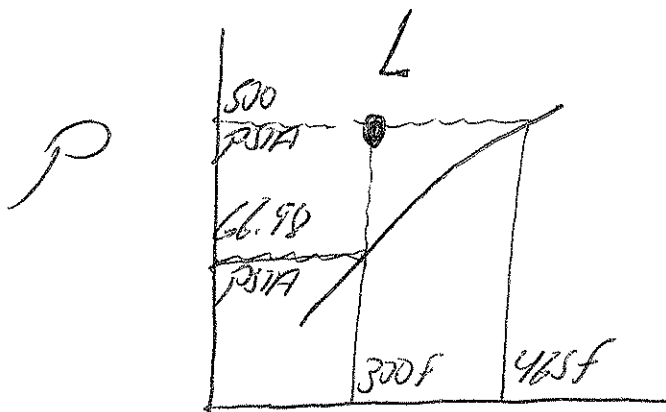
**GIVEN:** Water at  $p = 200$  psia,  $x = 0.36$   
**FIND:**  $v, h$

**GIVEN:** Ammonia at  $T = 200^\circ\text{F}$ ,  $h = 700$  Btu/lbm  
**FIND:**  $p$

**GIVEN:** R-22 at  $T = 10^\circ\text{F}$ ,  $p = 60$  psia  
**FIND:**  $v, u, h$

GIVEN: WATER @ 300F, 500 psia

FIND:  $v, \rho, u, h, s$



$$T_{sat} @ 500 \text{ psia (C.2a)}$$

BY interpolation...

$$T_{sat} \approx 465 \text{ F}$$

$$P_{sat} @ 300 \text{ F (C.1a)}$$

$$P_{sat} = 66.98 \text{ psia}$$

SINCE  $P > P_{sat} @ 300 \text{ F}$   
WE NEED TO USE C.9a  
(COMPRESSED LIQUID TABLE)

FROM C.9a 300F, 500 psia

$$v = 0.017416 \text{ FT}^3/\text{LBM}$$

$$\rho = 1/v = 57.418 \text{ LBM}/\text{FT}^3$$

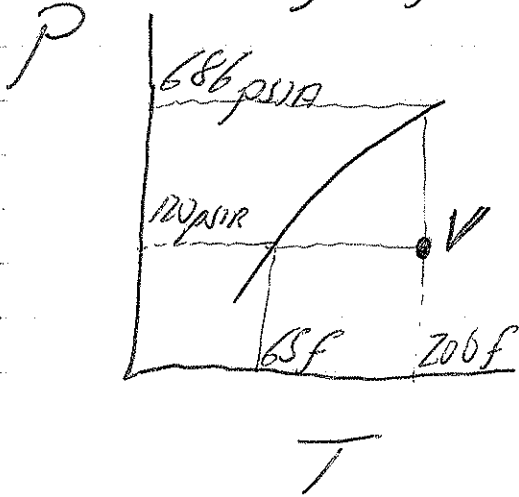
$$u = 268.92 \text{ BTU}/\text{LBM}$$

$$h = 270.53 \text{ BTU}/\text{LBM}$$

$$s = 0.43641 \text{ BTU}/\text{LBM} \cdot \text{R}$$

GIVEN:  $R_{22}$  @ 200 F, 120 psia

FIND:  $v$ ,  $u$ ,  $h$



$$T_{sat} @ 120 \text{ psia (C. 9a)}$$

$$T_{sat} \approx 65 \text{ F}$$

$$P_{sat} @ 200 \text{ F (C. 9a)}$$

$$P_{sat} \approx 686.36 \text{ psia}$$

FROM TABLE C. 10a

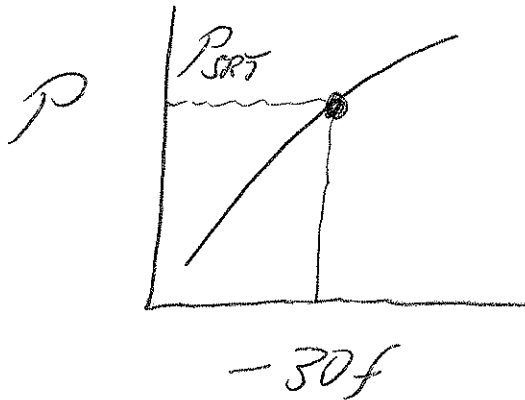
$$v = .64036 \text{ ft}^3/\text{lbm}$$

$$u = 121.16 \text{ BTU/lbm}$$

$$h = 135.38 \text{ BTU/lbm}$$

GIVEN: AMMONIA @ -30F

FIND: VAPOR PRESSURE AND  $h_{fg}$



FROM TABLE (C.S.G.)

$$P_{SAT} = 13.90 \text{ psia}$$

$$h_{fg} = 590.7 \text{ Btu/lbm}$$

(ALSO FROM  $h_f$  AND  $h_g$ )

$$h_g = 601.4 \text{ Btu/lbm}$$

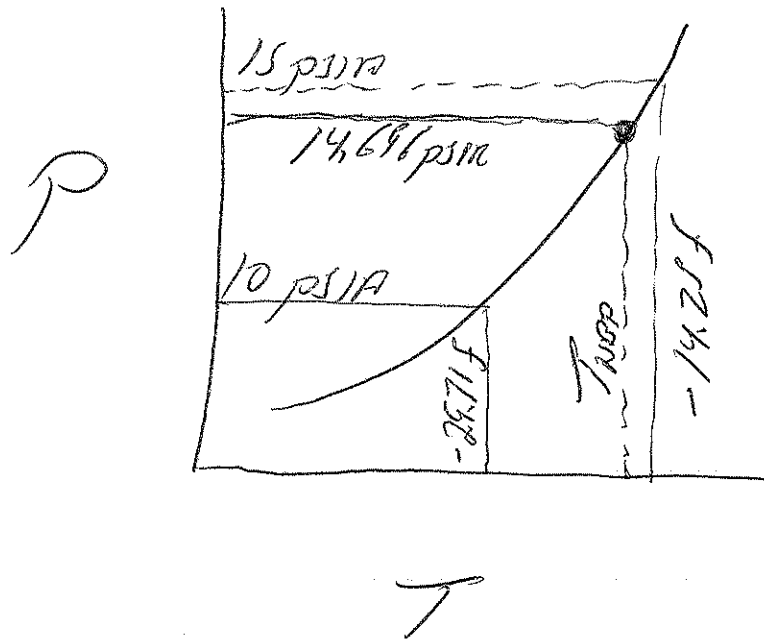
$$- h_f = -10.7 \text{ Btu/lbm}$$

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$$h_{fg} = 590.7 \text{ Btu/lbm}$$

GIVEN: TC-134a + NORMAL BOILING POINT

FIND:  $T_{NBP}$



NEED TO INTERPOLATE...

P (psia)	T (°F)
10	-29.71
14.696	$T_{NBP}$
15	-14.25

$$T_{NBP} = -29.71 F + (14.696 - 10) \text{psia} \frac{(-14.25 - (-29.71)) F}{(15 - 10) \text{psia}}$$
$$T_{NBP} = -75.19 F$$

GIVEN: WACC @ 200 psm,  $X = 0.36$

FIND:  $V, h$

$$V = (1-X) v_f + X v_g$$
$$V = 0.8358 \text{ Ft}^3/\text{lbm}$$

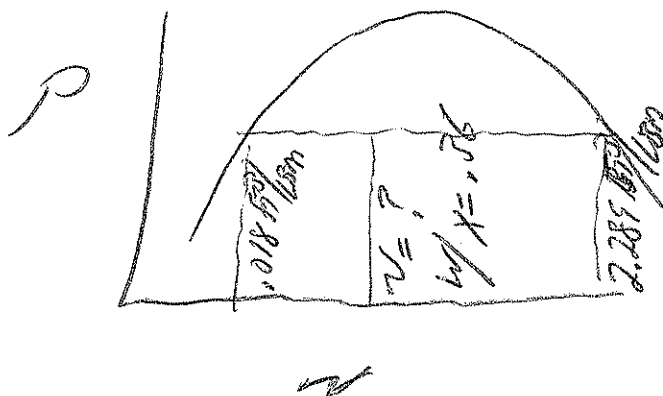
$$v_f = 0.01839 \text{ Ft}^3/\text{lbm}$$
$$v_g = 2.289 \text{ Ft}^3/\text{lbm}$$

$$h = (1-X) h_f + X h_g$$
$$h = 659.33 \text{ Btu/lbm}$$

$$h_f = 355.6 \text{ Btu/lbm}$$
$$h_g = 1199.3 \text{ Btu/lbm}$$

OR  $h = h_f + X h_{fg}$

$$h_{fg} = 843.7 \text{ Btu/lbm}$$



GIVEN: Ammonia @ 200°F,  $h = 700 \text{ Btu/lbm}$

FIND:  $P$

TABLE C.5a  $\rightarrow$  ONLY GOES TO 125°F

TABLE C.12a  $\rightarrow T_c = 729.8 \text{ R} = 270.13 \text{ °F}$

$\therefore$  C.5a IS ONLY R PROPER TABLE

SO, GO TO TABLE C.6a AND SCAN 200°F COLUMN

$h$ (Btu/lbm)	$P$ (psia)
701.9	220
700	$P?$
699.8	240

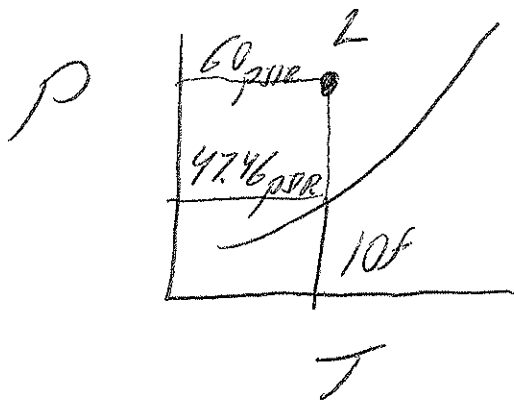
Interpolation...

$$P = 220_{\text{psia}} + (700 - 701.9) \frac{\text{Btu}}{\text{lbm}} \left( \frac{240 - 220}{699.8 - 701.9} \right)_{\text{psia}} \frac{\text{Btu}}{\text{lbm}}$$

$$P = \underline{\underline{238 \text{ psia}}}$$

GIVEN: R-22 @  $10^\circ\text{F}$ , 60 psia

FIND:  $v$ ,  $\mu$ ,  $h$



ISIT COMPRESSED  
LIQUID TABLE DON'T  
EXIST IN SUPPLEMENT!

ASSUME INCOMPRESSIBLE FLUID MODEL...

$$v = v_{sat} @ 10^\circ\text{F} = .01209 \text{ FT}^3/\text{LBM}$$

$$\mu = \mu_{sat} @ 10^\circ\text{F} = 13.00 \text{ BTU}/\text{LBM}$$

$$h_{sat} = \mu_{sat} + v_{sat} P_{sat} =$$

$$\frac{13.00 \text{ BTU}}{\text{LBM}} + \frac{.01209 \text{ FT}^3}{\text{LBM}} \left( \frac{47.46 \text{ LBF}}{\text{IN}^2} \right) \left( \frac{144 \text{ IN}^2}{\text{FT}^2} \right) \left( \frac{\text{BTU}}{778 \text{ FT-LBF}} \right)$$

$$h_{sat} = 13.10 \text{ BTU}/\text{LBM}$$

$$h(60 \text{ psia}) = h_{sat} + v_{sat} \Delta P$$

$$= 13.10 \frac{\text{BTU}}{\text{LBM}} + \left( \frac{.01209 \text{ FT}^3}{\text{LBM}} \right) (60 - 47.46 \text{ psia}) \left( \frac{144 \text{ IN}^2}{\text{FT}^2} \right) \left( \frac{\text{BTU}}{778 \text{ FT-LBF}} \right)$$
$$= 13.10 + .03 = \underline{\underline{13.13 \text{ BTU}/\text{LBM}}}$$